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# Short communication

# Ag/C nanoparticles as an cathode catalyst for a zinc-air battery with a flowing alkaline electrolyte

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# A R T I C L E I N F O

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# 1. Introduction

The development of fuel cells and metal-air batteries has aroused attention extensively in the world. As the cathode of battery, the oxygen electrode shows poor reversibility and is difficult to reduce, which becomes the major obstacle of battery reaction. How to raise  $O_2$  electrode activity is always one of the focal points in the fuel cell and metal-air battery fields. The overpotential produced by  $O_2$  reduction on the surface of traditional Pt/C catalysts is as high as 300–400 mV, and the performances of the fuel cell and metal-air battery are decreased [1–3]. Besides, Pt electrocatalysts are not only expensive, but also deficient in resource. Less expensive materials of carbon, manganese oxides [4–6] and composite compounds [7–9] are successfully used to replace expensive Pt metal as  $O_2$  electrode catalysts in alkaline medium.

The kinetics and mechanisms of  $O_2$  reduction have been investigated for a wide range of electrode materials and electrolytes. They rely greatly on the choice of active materials [10]. The reduction of  $O_2$  in alkaline electrolytes can be proceeded by two pathways [11], namely:

• Direct O<sub>2</sub> reduction to OH<sup>-</sup> ions, what is called four-electron pathway (I):

$$O_2 + 2H_2O + 4e^- \rightarrow 4OH^-$$
 (I)

# ABSTRACT

The cyclic voltammetry indicated that the oxygen reduction reaction (ORR) proceeded by the four-electron pathway mechanism on larger Ag particles (174 nm), and that the ORR proceeded by the four-electron pathway and the two-electron pathway mechanisms on finer Ag particles (4.1 nm), simultaneously. The kinetics towards ORR was measured at a rotating disk electrode (RDE) with Ag/C electrode. The number of exchanged electrons for the ORR was found to be close to four on larger Ag particles (174 nm) and close to three on finer Ag particles (4.1 nm). The zinc-air battery with Ag/C catalysts (25.9 nm) was fabricated and examined.

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• Or oxygen reduction to HO<sub>2</sub><sup>-</sup> ions, what is called two-electron pathway (II):

$$O_2 + H_2O + 2e^- \rightarrow HO_2^- + OH^-$$
 (II)

With subsequent reduction of peroxide ion to  $OH^-$  ions (III) or the decomposition of peroxide ion (IV):

$$HO_2^- + H_2O + 2e^- \rightarrow 3OH^-$$
 (III)

$$2HO_2^- \rightarrow 2OH^- + O_2 + 2e^-$$
 (IV)

Ag is one of the typical O<sub>2</sub> reduction catalysts, and has a reasonably high catalytic activity for O<sub>2</sub> reduction in alkaline electrolyte. Furthermore, it is a good catalyst for perhydroxyl ion decomposition [12,13]. Ag was used replacing Pt as O<sub>2</sub> reduction catalysts in fuel cell and metal-air battery in early stage. But Ag particles were easy to accumulate into larger particles in the process of preparation. this would reduce catalytic activity of Ag. Afterwards Ag was adopted rarely. The key to the preparation of Ag catalysts lies in raising the specific surface area of Ag as far as possible [14,15]. Many studies have been reported on the kinetics of O<sub>2</sub> reduction on a bulk Ag electrode, but the ORR seems to vary considerably [14,16–18]. It is reported that the  $O_2$  reduction proceeds by the four-electron pathway mechanism on the surface of the Ag/C electrode [13,14,19]. In the previous work, we synthesized the single crystal of [Ag(L)(bbi)] (L=2-amino-3,5-dimethylbenzenesulf-onate anion, bbi = 1,1'-(butane-1,4-diyl)diimidazole) [20]. Ag/C catalysts with different contents of Ag were prepared and physically characterized using the [Ag(L)(bbi)] by Ag(I) single crystal reduction method (Ag(I) SCRM). The Ag(I) single crystal reduction is the method of the reduction of Ag(I) ions in single crystals to Ag metal

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using NaBH<sub>4</sub> as reductant. Their electrochemical performances were investigated by using Ag/C as  $O_2$  reduction electrocatalysts in alkaline electrolyte. The electrocatalytic activity of Ag/C catalysts prepared by Ag(I) SCRM is significantly enhanced compared with that of Ag/C catalysts prepared by Ag<sub>2</sub>O reduction method (Ag<sub>2</sub>O RM) under the same content of Ag [21]. In this study, the rotating disk electrode (RDE) method and the cyclic voltammetry were used to study the kinetics and mechanism of  $O_2$  electrode reactions, using Ag/C as the catalysts prepared by Ag(I) SCRM was examined.

# 2. Experimental

#### 2.1. Preparation of air electrodes

A rotating disc electrode with a glassy carbon electrode (5 mm diameter) was used. Ag/C catalysts were dispersed in 0.1 wt.% polytetrafluoroethylene (PTFE) solution (Cabot, US) and resultant suspension was agitated in an ultrasonic bath for 30 min. The suspension was coated on the glassy carbon electrode, which was air-dried for 1 h. Ag/C electrodes for a three-electrode cell were prepared. 1.5 g of Ag/C catalysts was weighed and added to 0.5 ml of 50 wt.% PTFE solution, the mixture was mixed fully and pressed into a round sheet of 2.0 cm in diameter. The nickel net was pressed onto one side of the round sheet, and a thin layer of PTFE film was coated evenly on another side. Ag/C electrodes prepared were dried in a vacuum drying oven at 40 °C for 72 h. The cathode of the zinc-air battery was prepared using 10 wt.%Ag/C (25.9 nm) prepared by the Ag(I) SCRM as the catalysts according to the steps detailed in [21]. Ag loading of the cathode was  $30 \text{ mg cm}^{-2}$ . The carbon support used was VulcanXC-72R carbon (produced by Cabot, US), and its BET area was  $254 \text{ m}^2 \text{ g}^{-1}$ .

# 2.2. Cyclic voltammetry

The reduction of  $O_2$  from air was studied in a three-electrode cell (made of PMMA organic glass) that contained a Pt counter electrode, a Hg/HgO, OH<sup>-</sup> reference electrode and a Ag/C electrode as a working electrode. The electrolyte was 5.0 mol L<sup>-1</sup> KOH aqueous solution. Cyclic voltammograms were conducted with a CHI660A electrochemical workstation system (Shanghai Chenhua Instrument Company). The experiments were performed over the potential range of -0.4 to 1.3 V at a scanning rate of 10 mV s<sup>-1</sup>.

#### 2.3. Measurement of the kinetics

The kinetics of oxygen reduction was studied in  $O_2$ -saturated 1.0 mol L<sup>-1</sup> KOH solution in a three-electrode cell (made of PMMA organic glass) with the Ag/C glassy carbon electrode as the working electrode, Hg/HgO, OH<sup>-</sup> electrode as the reference electrode, and platinum spiral wire as the auxiliary electrode. The electrochemical measurements were performed by the CHI660A electrochemical workstation system (Shanghai Chenhua Instrument Company) and the rotation rates were controlled by the AFMSRXB Model Analytical Rotator (Pine Instrument Company, USA).

#### 2.4. Measurement of the polarization

The anode of the zinc-air battery was an zinc electrode which contained automatic packed cuneiform bed (right inverted trapezoid shaped chamber) made of the nickel mesh. The case of battery was made of PMMA organic glass. The area of the electrode in one side was  $5.0 \text{ cm} \times 3.0 \text{ cm}$ . The upper slit of the cuneiform trough was 3.0 mm in width and the lower slit was 0.5 mm in width. The zinc



Fig. 1. Schematic diagram of the zinc-air battery.

grains (1.0 mm diameter) were used as the fuel. Under the action of gravity, the zinc grains automatically entered the cuneiform trough from the upper slit with the flowing electrolyte. The discharge products (ZnO) of zinc were carried by the flowing electrolyte from the lower slit. A schematic diagram of the zinc-air battery is shown in Fig. 1. The polarization data of the battery and electrodes were recorded at a constant current using a LK2000B charge–discharge system (Tianjin LK Company). The flowing alkaline electrolyte was  $6.5 \text{ mol } \text{L}^{-1}$  KOH aqueous solution (2.0 ml min<sup>-1</sup>) and the reference electrode was a Hg/HgO, OH<sup>-</sup> electrode.

# 3. Results and discussions

#### 3.1. Mechanism of the ORR

Cyclic voltammograms were repeated five times for a wide range of potential sweeps for the electrode with 20 wt.%Ag/C catalysts (174 nm) prepared by Ag<sub>2</sub>O RM in alkaline electrolyte in Fig. 2. The current peak observed at -0.17 V corresponds to the O<sub>2</sub> reduction reaction. The single reduction potential peak supports the four-electron pathway mechanism.



**Fig. 2.** Cyclic voltammetric curves for O<sub>2</sub> on the electrode with 20 wt.%Ag/C catalysts prepared by Ag<sub>2</sub>O RM in 5.0 mol  $L^{-1}$  KOH at a scanning rate of 10 mV s<sup>-1</sup> (the active area of the electrode: 3.0 cm<sup>2</sup>; Ag loading: 300 mg).



**Fig. 3.** Cyclic voltammetric curve for  $O_2$  on the electrode with 0.5 wt.%Ag/C catalysts prepared by Ag(I) SCRM in 5.0 mol  $L^{-1}$  KOH at a scanning rate of 10 mV s<sup>-1</sup> (the active area of the electrode:  $3.0 \text{ cm}^2$ ; Ag loading: 7.5 mg).

Fig. 3 shows cyclic voltammogram for the electrode with 0.5 wt.%Ag/C catalysts (4.1 nm) prepared by Ag(I) SCRM in alkaline electrolyte. The current peaks observed at 0.09 and -0.23 V correspond to the O<sub>2</sub> reduction reaction. The two reduction potential peaks support the four-electron pathway and the two-electron pathway mechanisms, simultaneously.

Therefore it can be deduced that the ORR proceeds by the four-electron pathway mechanism on larger Ag particles (174 nm), and that the ORR proceeds by the four-electron pathway and the two-electron pathway mechanisms on finer Ag particles (4.1 nm), simultaneously.

## 3.2. Kinetic of oxygen reduction

The RDE method was used to study the kinetics of air electrode reaction through a Koutecky–Levich plot. According to the Levich and Koutecky–Levich equations:

$$i_{\rm L} = 0.620 n F A D_0^{2/3} \omega^{1/2} \nu^{-1/6} C_0 \tag{1}$$

$$i_{\rm K} = nFAK\Gamma_{\rm cat}C_0 \tag{2}$$

$$i^{-1} = i_{\rm K}^{-1} + i_{\rm L}^{-1} \tag{3}$$

$$i^{-1} = \frac{1}{(nFAK\Gamma_{cat}C_0)} + \frac{1}{0.620nFAD_0^{2/3}\nu^{-1/6}C_0\omega^{1/2}}$$
(4)

where  $i_L$  (A) is the limiting current for the electrode reaction of reactive species by the diffusion controlled process,  $i_K$  (A) is the kinetic current for the reaction of reactive species at the electrode surface,  $n \,(\text{mol}^{-1})$  is the electron transfer number per mole of reactive species,  $F(C \,\text{mol}^{-1})$  is Faraday constant (=96,500 C  $\text{mol}^{-1})$  [22],  $A \,(\text{cm}^2)$  is the electrode area,  $D_0 \,(\text{cm}^2 \,\text{s}^{-1})$  is the diffusion coefficient of  $O_2$  in 1 mol L<sup>-1</sup> KOH solution (=1.76 × 10<sup>-5</sup> cm<sup>2</sup> s<sup>-1</sup>) [22],  $\omega \,(\text{s}^{-1})$  is the rotation rate,  $\nu \,(\text{cm}^2 \,\text{s}^{-1})$  is the kinetic viscosity of water (=0.01 cm<sup>2</sup> s<sup>-1</sup>) [22],  $C_0 \,(\text{mol L}^{-1})$  is the concentration of  $O_2$  in 1 mol L<sup>-1</sup> KOH solution at 25 °C (=1.103 × 10<sup>-3</sup> mol L<sup>-1</sup>) [22],  $K \,(\text{M}^{-1} \,\text{s}^{-1})$  is the kinetic rate constant for catalytic reaction, and  $\Gamma_{\text{cat}} \,(\text{mol cm}^{-2})$  is the quantity of catalyst on the surface of the electrode (=9.26 × 10<sup>-5</sup> mol cm<sup>-2</sup>).

Fig. 4 shows the curves of the current–potential for  $O_2$  reduction at the electrode with 20 wt.%Ag/C catalysts prepared by Ag<sub>2</sub>O RM at different rotation rates. The current of  $O_2$  reduction increases with increasing rotation rates. Fig. 5 shows the Koutecky–Levich plots obtained from the data in Fig. 4. The analysis results of ORR kinetic were summarized in Table 1. The number of exchanged electrons for the ORR was found to be close to four. It is concluded that the ORR is



**Fig. 4.** Curves of the current–potential for O<sub>2</sub> reduction at different rotation rates on a glassy carbon electrode with 20 wt.%Ag/C catalysts prepared by Ag<sub>2</sub>O RM in 1.0 mol L<sup>-1</sup> KOH (the active area of the electrode:  $0.2 \text{ cm}^2$ ; Ag loading: 2 mg).



Fig. 5. Koutecky-Levich plots for 20 wt.%Ag/C catalysts prepared by Ag<sub>2</sub>O RM at different potentials.

a direct four-electron process. With increasing electrode potential the rate constant increases.

Fig. 6 shows the curves of the current–potential for  $O_2$  reduction at the electrode with 0.5 wt.%Ag/C catalysts prepared by Ag(I) SCRM at different rotation rates. The current of  $O_2$  reduction increases with increasing rotation rates. Fig. 7 shows the Koutecky–Levich plots obtained from the data in Fig. 6. The analysis results of ORR kinetic were summarized in Table 2. The number of exchanged electrons for the ORR was found to be close to three. It is concluded that the ORR proceeds by the four-electron pathway and the two-electron pathway, simultaneously. With increasing electrode potential the rate constant increases.

From Figs. 5 and 7, under the same Ag loadings (2 mg), the current increases with decreasing Ag particle sizes. This indicated that

#### Table 1

Kinetic parameters for catalytic reduction of oxygen at a glassy carbon electrode with 20 wt.%Ag/C catalysts prepared by  $Ag_2O$  RM (Ag loading: 2 mg).

<i>E/V</i> (vs. Hg/HgO, OH <sup>-</sup> )	20 wt.%Ag/C catalysts (particle-size of Ag: 174 nm)		
	Slope (×10 <sup>3</sup> )	<i>n</i> (mol)	$K(\times 10^2 \text{ M}^{-1} \text{ s}^{-1})$
0.5	5.45	3.80	6.3
0.6	5.57	3.72	7.4
0.7	5.40	3.83	8.6
0.8	5.35	3.87	9.7
0.9	4.97	3.75	10.7



Fig. 6. Curves of the current-potential for O<sub>2</sub> reduction at different rotation rates on a glassy carbon electrode with 0.5 wt.%Ag/C catalysts prepared by Ag(I) SCRM in 1.0 mol  $L^{-1}$  KOH (the active area of the electrode:  $0.2 \text{ cm}^2$ ; Ag loading: 2 mg).



Fig. 7. Koutecky-Levich plots for 0.5 wt.%Ag/C catalysts prepared by Ag(I) SCRM at different potentials.

the electrocatalytic activity was enhanced with increasing specific surface area of Ag.

#### 3.3. Polarization curves of electrodes

Fig. 8 shows the polarization curves of electrodes obtained for the zinc-air battery in the temperature range between 35 °C and 80°C. The curves indicated that the zinc-air battery is cathode-limited. The polarization of the cathode decreases with increasing temperature. This could be due to the increased reaction kinetics.

#### 3.4. Polarization curves of the battery

Fig. 9 shows the polarization curves of the zinc-air battery obtained at different temperature. With increasing temperature the

#### Table 2

Kinetic parameters for catalytic reduction of oxygen at a glassy carbon electrode with 0.5 wt.%Ag/C catalysts prepared by Ag(I) SCRM (Ag loading: 2 mg).

<i>E/V</i> (vs. Hg/HgO, OH <sup>-</sup> )	0.5 wt.%Ag/C catalysts (particle-size of Ag: 4.1 nm)			
	Slope (×10 <sup>3</sup> )	n (mol)	$K(\times 10^2 \mathrm{M}^{-1} \mathrm{s}^{-1})$	
0.5	7.03	2.94	18.3	
0.6	7.36	2.81	21.4	
0.7	7.26	2.85	25.9	
0.8	6.90	2.99	38.1	
0.9	6.80	2.90	40.9	



Fig. 8. Polarization curves of the anode and cathode in 6.5 mol L<sup>-1</sup> KOH (the active area of the electrode: 30 cm<sup>2</sup>; Ag loading: 30 mg cm<sup>-2</sup>; measurement time: 1 min per point).



Fig. 9. Polarization curves of the zinc-air battery in 6.5 mol L<sup>-1</sup> KOH (the active area of the electrode: 30 cm<sup>2</sup>; Ag loading: 30 mg cm<sup>-2</sup>; measurement time: 1 min per point).

power density increases. Power densities of 34 mW cm<sup>-2</sup> at 35 °C and 72 mW cm<sup>-2</sup> at 80 °C have been obtained.

## 4. Conclusions

The ORR proceeds by the four-electron pathway and the twoelectron pathway on Ag/C catalysts, simultaneously. The larger Ag particles are favourable to the four-electron reduction of  $O_2$ ; the finer Ag particles are favourable to the two-electron reduction of O<sub>2</sub>. The zinc-air battery has the power densities of 34 mW cm $^{-2}$  at 35  $^{\circ}$ C and 72 mW cm<sup>-2</sup> at 80 °C with 10 wt.%Ag/C (25.9 nm) prepared by the Ag(I) SCRM as catalysts.

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